2. Chemical and Phase Equilibria

(Gas-phase Chemical Equilibrium)

In the equilibrium state of a gas-phase reaction, $A(g) + B(g) \rightleftharpoons C(g)$,

$$\mu[C(g)] = \mu[A(g)] + \mu[B(g)]$$
 (2.1)

The chemical potential of an ideal gas A at a partial pressure p_A is,

$$\mu[A(g)] = \mu^{\circ}[A(g)] + RT \ln \frac{p_A}{p^{\circ}}$$
 (0.6)

Similar relation holds for gas B and C. The standard Gibbs energy change of this reaction is

$$\Delta_{r}G^{\circ} = \mu^{\circ} [C(g)] - \mu^{\circ} [A(g)] - \mu^{\circ} [B(g)]$$
 (2.2)

Exercise 2.1

- 1) Derive an equation for the relation among p_A , p_B , p_C , and $-\Delta_r G$ for $A(g) + B(g) \rightleftharpoons C(g)$.
- 2) Calculate the equilibrium constant for the reaction, $H_2(g) + \frac{1}{2}O_2(g) \rightleftharpoons H_2O(g)$, at 3000 K from the following data.

$$T/K$$
 $\Delta_f G^{\circ}[H_2O(g)]/kJ \text{ mol}^{-1}$ [JANAF] 3000 -77.2

Solution to Exercise 2.1

1) Substitution of (0.6) to (2.1) and transformation give

$$RT \ln \frac{p_{\rm C} / p^{\circ}}{(p_{\rm A} / p^{\circ})(p_{\rm B} / p^{\circ})} = \mu^{\circ} [A(g)] + \mu^{\circ} [B(g)] - \mu^{\circ} [C(g)]$$

By using (2.2),
$$RT \ln K = -\Delta_r G^\circ$$
, where $K \equiv \frac{p_C / p^\circ}{(p_A / p^\circ)(p_B / p^\circ)}$

2) $K = \exp(-\Delta_r G^{\circ} / RT) = \exp[77.2 \times 1000 / (8.3145 \times 3000)] = 22.09 [-] (or bar^{-1/2})$

(Phase Equilibrium between Condensed Phases)

On the boundary between phase 1 and 2 in p–T plane,

$$\mathrm{d}\mu(1) = \mathrm{d}\mu(2) \tag{2.3}$$

From (0.3) and (0.4), one obtains $V_{\rm m}(1)\mathrm{d}p - S_{\rm m}(1)\mathrm{d}T = V_{\rm m}(2)\mathrm{d}p - S_{\rm m}(2)\mathrm{d}T$, and then,

$$\frac{\mathrm{d}p}{\mathrm{d}T}\Big|_{\mathrm{phase\ boundary}} = \frac{\Delta_{\mathrm{trs}}S}{\Delta_{\mathrm{trs}}V}$$
 (Clapeyron equation) (2.4)

where
$$\Delta_{\text{trs}}S = S_{\text{m}}(2) - S_{\text{m}}(1)$$
, $\Delta_{\text{trs}}V = V_{\text{m}}(2) - V_{\text{m}}(1)$

From the definition of the entropy,

$$\Delta_{\rm trs}S = \frac{\Delta_{\rm trs}H}{T_{\rm tre}} \tag{2.5}$$

Exercise 2.2

- 1) Calculate the standard entropy of fusion $\Delta_{\text{fus}}S^{\circ}$ of the ice from the standard enthalpy of fusion, $\Delta_{\text{fus}}H^{\circ} = 6.008 \text{ kJ mol}^{-1}$, at 0 °C.
- 2) Estimate the melting point of ice at a pressure 136 bar from the $\Delta_{fus}S$ above and the following densities of ice and water. Ignore the pressure dependence of $\Delta_{fus}S$ and density.

	ρ (273.15 K, 1 bar) / g cm ⁻³	
$H_2O(1)$	0.9998	
$H_2O(s)$	0.9168	

Solution to Exercise 2.2

- 1) $\Delta_{\text{fus}} S^{\circ} = 6.008 \times 1000 / 273.15 = 22.00 \text{ J K}^{-1} \text{ mol}^{-1}$
- 2) $\Delta_{\text{fus}}V^{\circ} = (18.02/0.9998) (18.02/0.9168) = -1.632 \text{ cm}^3 \text{ mol}^{-1} = -1.632 \times 10^{-6} \text{ m}^3 \text{ mol}^{-1}$ $\text{d}T/\text{d}p\mid_{\text{boundary}} = -1.632 \times 10^{-6} / 22.00 = -7.418 \times 10^{-8} \text{ K Pa}^{-1} = -7.418 \times 10^{-3} \text{ K bar}^{-1}$ $\text{d}T = -7.418 \times 10^{-3} \times (136 - 1) = -1.00 \text{ K}$ $\Rightarrow \tau T_{\text{fus}}(136 \text{ bar}) \sim -1.00 \text{ °C } (272.15 \text{ K})$

(Phase Equilibrium between Gas and Condensed Phases)

On the boundary between a condensed phase 1 and a gas phase,

$$\mu(1) = \mu(g) \tag{2.6}$$

By ignoring the small pressure dependence of the chemical potential of a condensed phase, and using (0.6),

$$-\Delta_{\text{vap}}G^{\circ} = \mu^{\circ}(1) - \mu^{\circ}(g) = RT \ln(p/p^{\circ})$$
(2.7)

Exercise 2.3

1) Calculate the vapor pressure of water at 298 K from the following data.

(298 K)	$\Delta_{\rm f} H^{\circ} / {\rm kJ \ mol}^{-1}$	$S_{\rm m}^{\circ}$ / J K ⁻¹ mol ⁻¹
H ₂ O(l)	-285.8	69.9
H ₂ O(g)	-241.8	188.8

2) Estimate the vapor pressure of water at 100 °C (= 373 K) assuming that $\Delta_{\text{vap}}H^{\circ}$ and $\Delta_{\text{vap}}S^{\circ}$ are independent of temperature.

Solution to Exercise 2.3

- 1) $\Delta_{\text{vap}}H^{\circ} = -241.8 (-285.8) = 44.0 \text{ kJ mol}^{-1}$, $\Delta_{\text{vap}}S^{\circ} = 188.8 69.9 = 118.9 \text{ J K}^{-1} \text{ mol}^{-1}$ $\Delta_{\text{vap}}G^{\circ} = \Delta_{\text{vap}}H^{\circ} - T\Delta_{\text{vap}}S^{\circ} = 44.0 - 298 \cdot 118.9 / 1000 = 8.57 \text{ kJ mol}^{-1}$ $p / p^{\circ} = \exp(-8.57 \times 1000 / 8.3145 \cdot 298) = 3.15 \times 10^{-2}$, thus p = 0.0315 bar
 - * The pressure dependence of $\mu[H_2O(1)]$ is, from (0.9), $V_m(p-p^\circ) = 1.8 \times 10^{-5} (3160-100000) = -1.7 \text{ J mol}^{-1}$, which is smaller than the smallest significant digit of $\Delta_f G^\circ$.
- 2) $\Delta_{\text{vap}}G^{\circ} = \Delta_{\text{vap}}H^{\circ} T\Delta_{\text{vap}}S^{\circ} = 44.0 373 \cdot 118.9/1000 = -0.35 \text{ kJ mol}^{-1}$ $p/p^{\circ} = \exp(+0.35 \times 1000 / 8.3145 \cdot 373) = 1.119$, thus p = 1.119 bar (10% higher than 1 atm!)